# Techno-economic and ecological evaluation of a wood biorefinery

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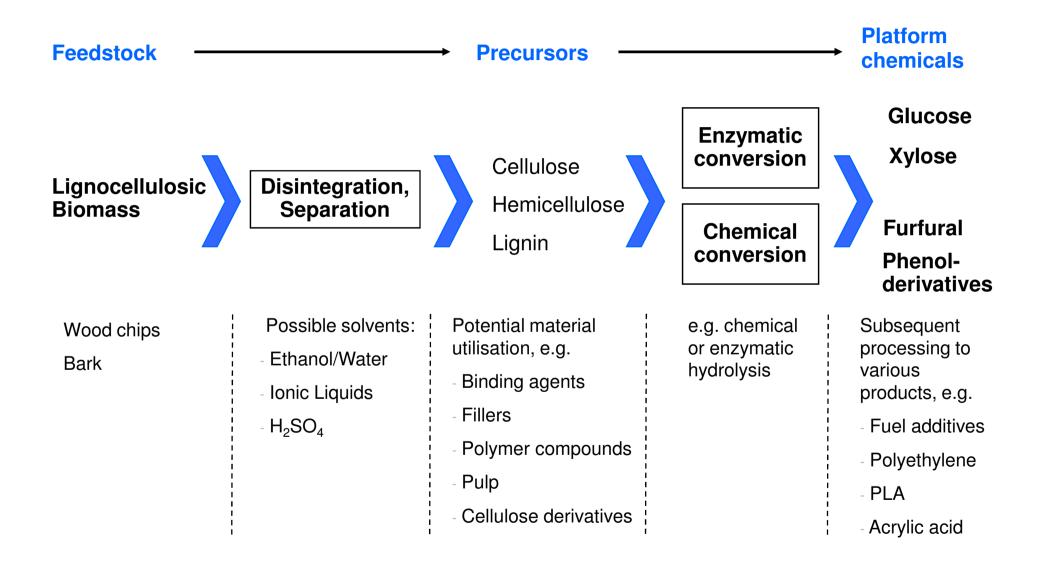
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#### Increasing use of biomass in fossil based industries

- Replacement of limited fossil raw materials
- Increasing prices for non-renewable raw materials
- Reduction of dependency on crude oil imports and securing of raw material supply
- Reduction of greenhouse gas emissions
- ⇒ Increase of competition for biomass and arable land through new biomass utilization concepts
- ⇒ Enhancement of research and development regarding new conversion technologies

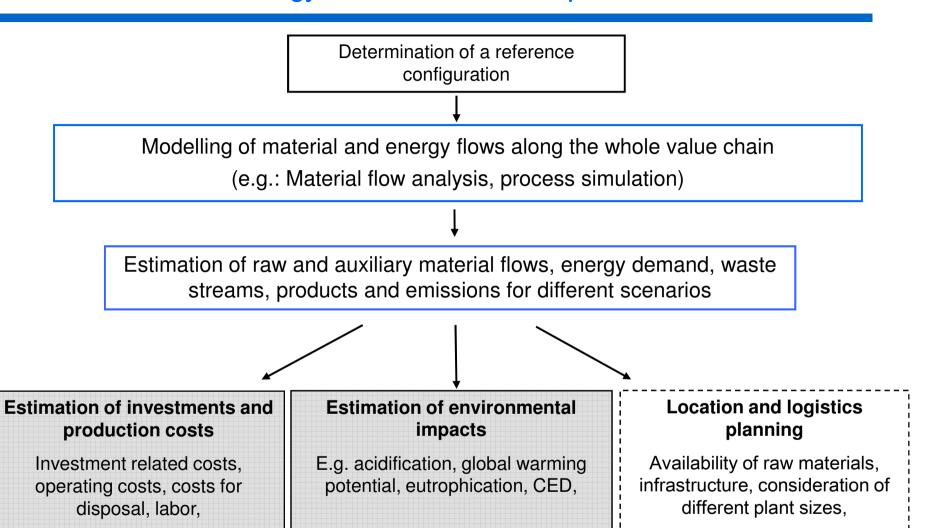
## Possible process steps and potential products of a wood biorefinery



#### Objectives of the techno-economic and ecological evaluation

- Estimation of production costs and environmental effects of a process chain for the use of biomass at an early stage of process development
- Determination of economic and ecological key parameters and their influence on the sustainability of the process chain
- Identification of cost-effective and environmentally sound process configurations

#### Methodology for the evaluation of process chains



Sensitivity analysis

#### Reference configuration of the modelled biorefinery

Plant capacity: 400.000 t dry wood/year

Load: 50 t drv wood/h (8000 h/year)

Feedstock properties: Wood chips of residual wood (P100, 50% water content),

42 % cellulose, 29% hemicellulose, 24% lignin, 5% others

Organosolv pulping: Ethanol/Water mixture (50/50)

 $T = 180^{\circ}C$ , p = 18bar

Ratio wood: solvent = 1:6

Enzymatic conversion of cellulose: Conversion rate to glucose: 82%

Cellulase and beta-glucosidase enzymes

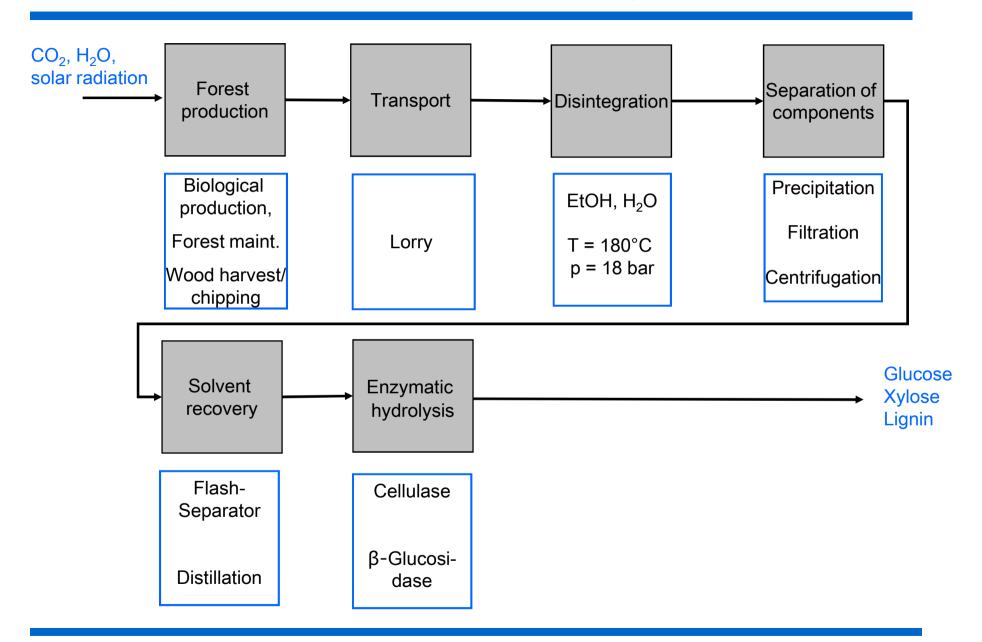
Hemicellulose fraction: Solute hemicellulose fragments after

organosoly pulping are subsumed to xylose

Final products:

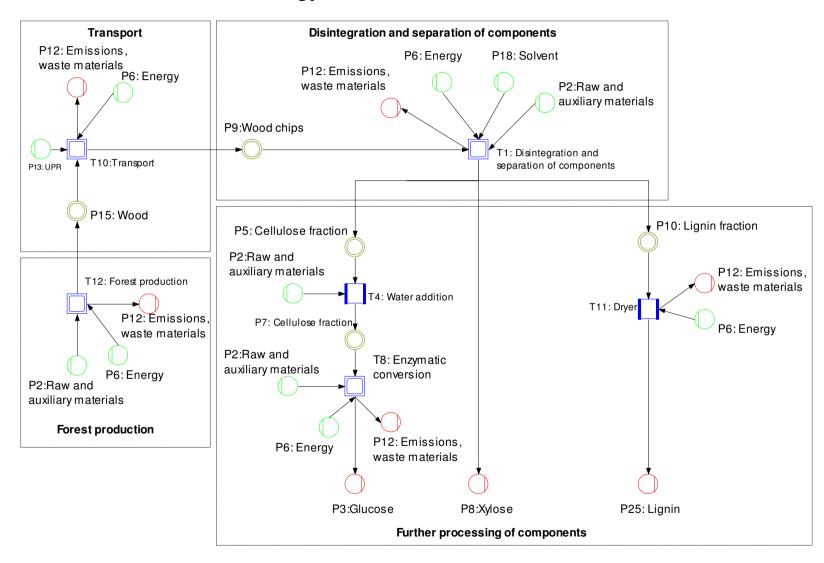
Main product: Glucose (solution ~16 mass-%), Byproducts: Xylose (solution ~5 mass-%), lignin (dry)

## Major process steps for the production of glucose from wood

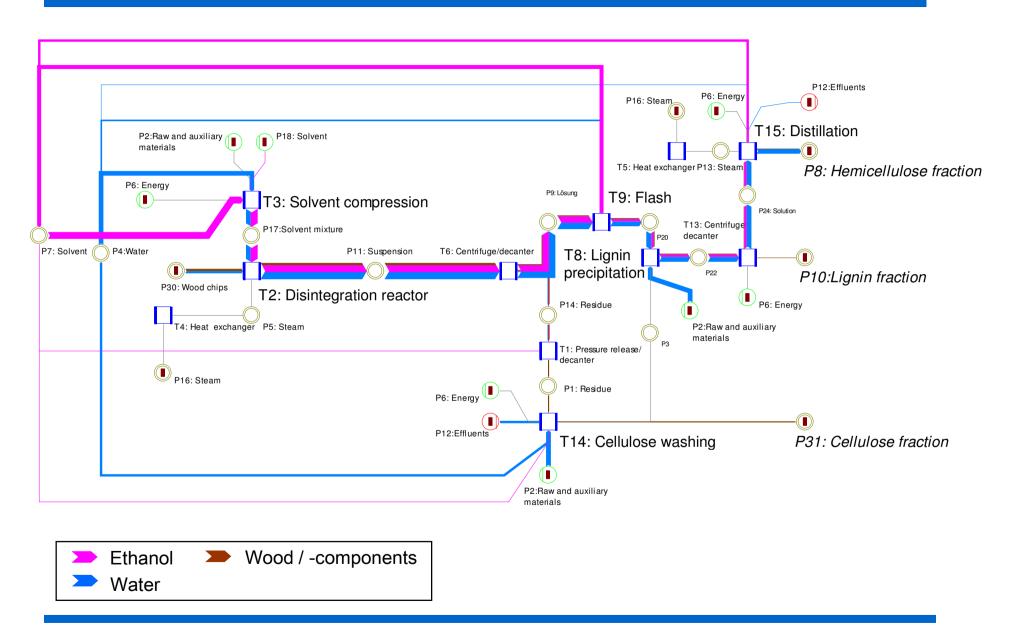


## Modelling of material and energy flows along the whole value chain

#### ■ Umberto® material and energy flow network



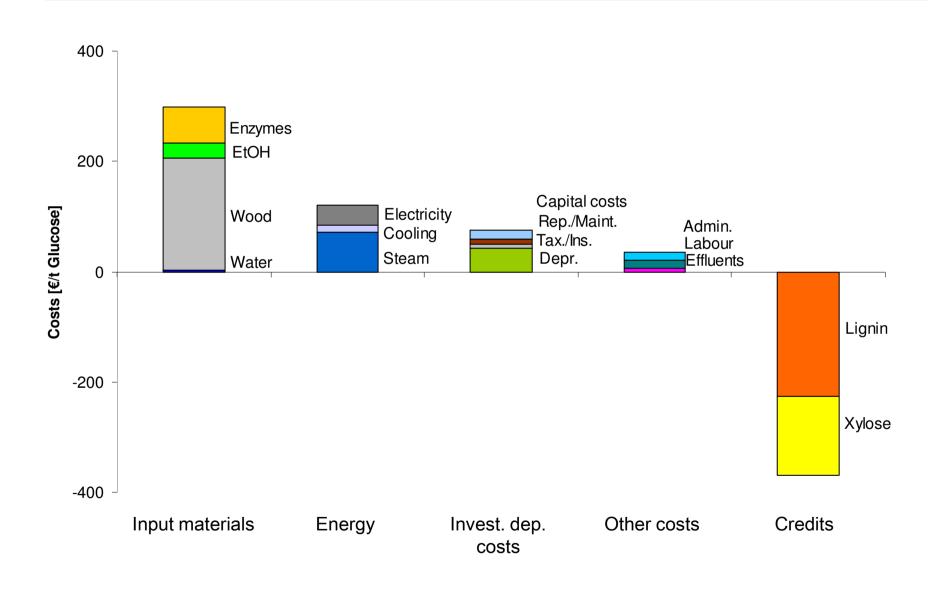
## Subnet "Disintegration and separation of components" (Sankey Diagram)



#### Methodology for economic analysis

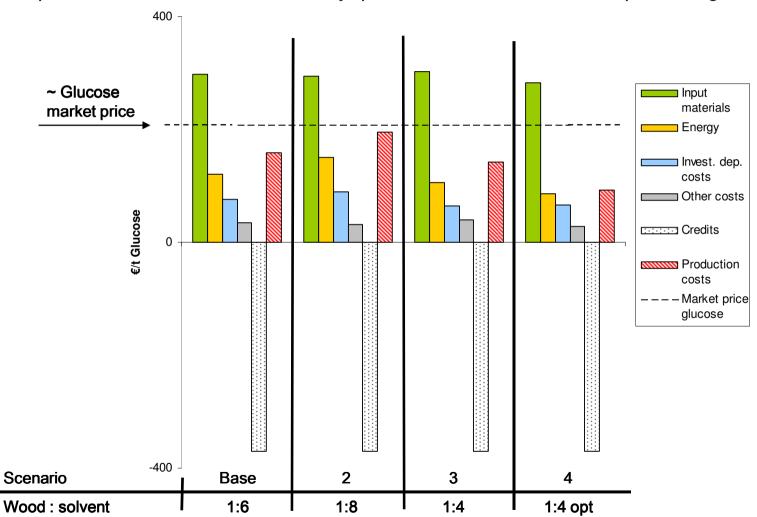
- Estimation of investments:
  - +/- 30% accuracy
  - Site infrastructure completely available and useable (outside battery limits neglected)
- Determination of glucose production costs:
  - Variable costs and credits
    - Costs for raw and operating materials (wood chips, ethanol, water, enzymes)
    - Energy costs (electricity, steam, cooling)
    - Costs for sewage disposal
    - Credits for by-products (lignin as high grade product, xylose)
  - Investment related costs (depreciations, taxes and insurance, reparation and maintenance, costs of capital)
  - Labour costs
- Costs for sales, administration and research are not yet determined

#### Structure of costs and credits for the base scenario



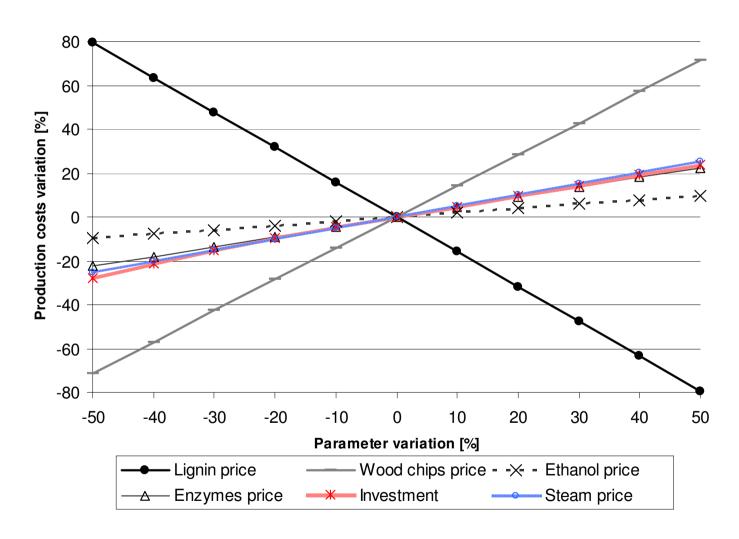
## Estimation of glucose production costs for different scenarios

- Consideration of different wood : solvent ratios
- Requirement for economic efficiency: production costs << market price for glucose



## Sensitivity analysis for the base scenario

■ Prices for wood chips and lignin mainly influence glucose production costs

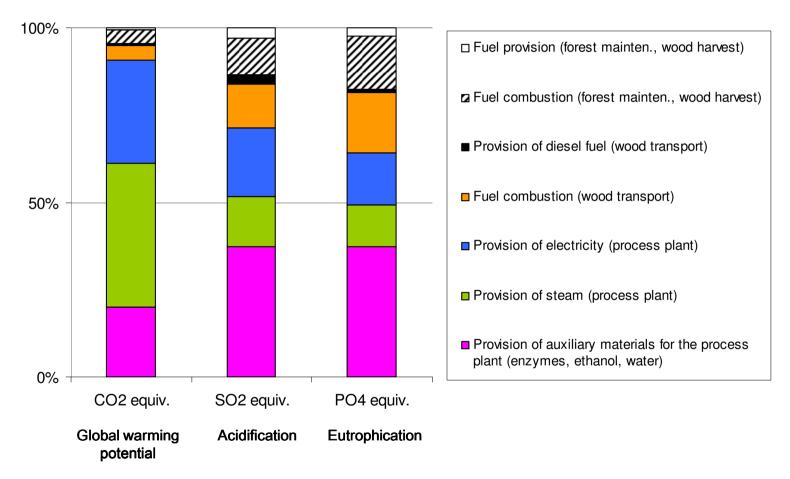


#### Methodology for ecological evaluation

- Methodology for life cycle assessment (LCA) according to the international standard DIN EN ISO 14040 and 14044
- Goal and scope definition and life cycle inventory analysis
  - "Cradle to gate analysis" including forest production (wood maintenance, wood harvest/chipping), wood transport and the biorefinery processes
  - Integration of supply chains for the provision of energy and operating materials (ecoinvent v2.0 LCl database)
- Selection of impact categories, e.g. global warming potential, acidification, eutrophication
- Life cycle impact assessment (e.g. allocation of emissions to the corresponding impact categories and conversion to indicator values, e.g. CO<sub>2</sub> equivalents)

## Ecological evaluation – Examples (1)

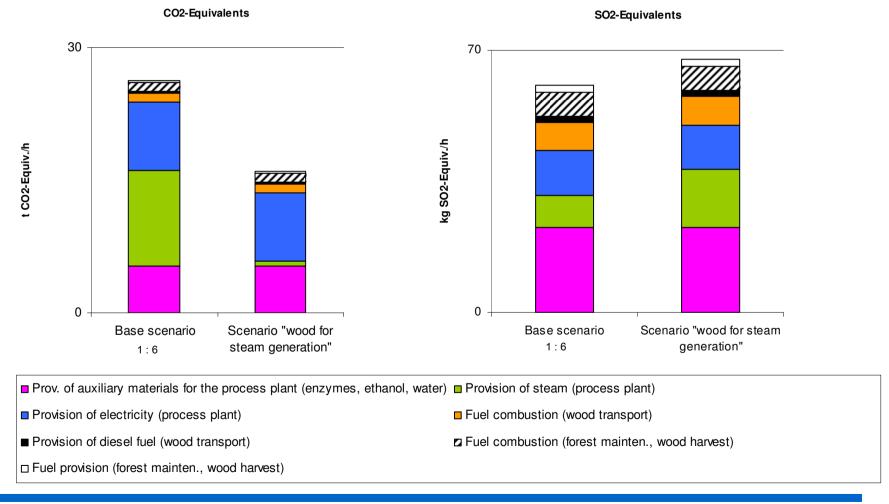
 Determination of proportions of particular process steps to the emission equivalents of selected impact categories (base scenario)



■ Uncertainties for contributions caused by enzymes production especially for PO<sub>4</sub>-Eq.

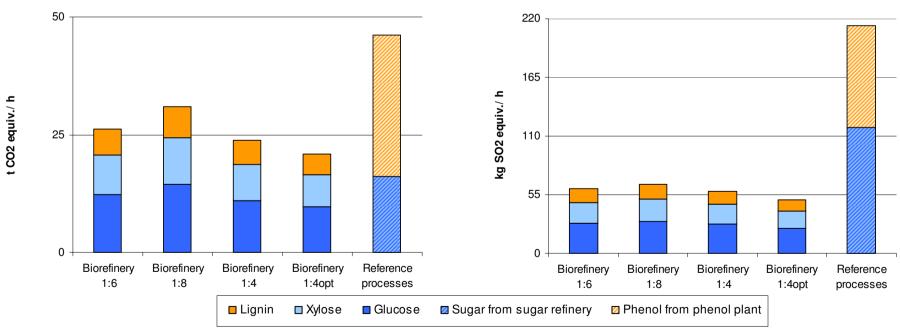
## Ecological evaluation – Examples (2)

- Comparision of indicator values (CO<sub>2</sub>- and SO<sub>2</sub>- equivalents) for different scenarios
- Different scenarios result in different conclusions for several impact categories



## Ecological evaluation – Examples (3)

- Comparison of CO<sub>2</sub>- and SO<sub>2</sub>- equivalents of the biorefinery with the production of potential reference products
- Assumptions:
  - Sugar from a sugar refinery as reference product for xylose and glucose
  - Phenol from a phenol plant as reference product for lignin
- Consideration of different wood : solvent ratios
- Biorefinery causes lower environmental effects compared to the reference processes<sup>1</sup>



<sup>&</sup>lt;sup>1</sup> Values for reference processes derived from the ecoinvent v2.0 LCI database

#### **Summary**

- Development of new concepts for the non-energetic use of biomass, e.g. wood biorefineries producing platform chemicals
- Modelling of mass and energy flows of a wood biorefinery along the whole value chain for different scenarios
- Early-stage techno-economic and ecological evaluation for the identification of sustainable production processes
- Economic efficiency highly depends on prices for raw materials and the sales price for lignin
- Further improvement of process design is necessary to enhance economic efficiency
- Steam and electricity generation are crucial for the extent of GHG emissions
- Analysis of different impact categories may lead to different conclusions

# Thank you for your attention!



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