



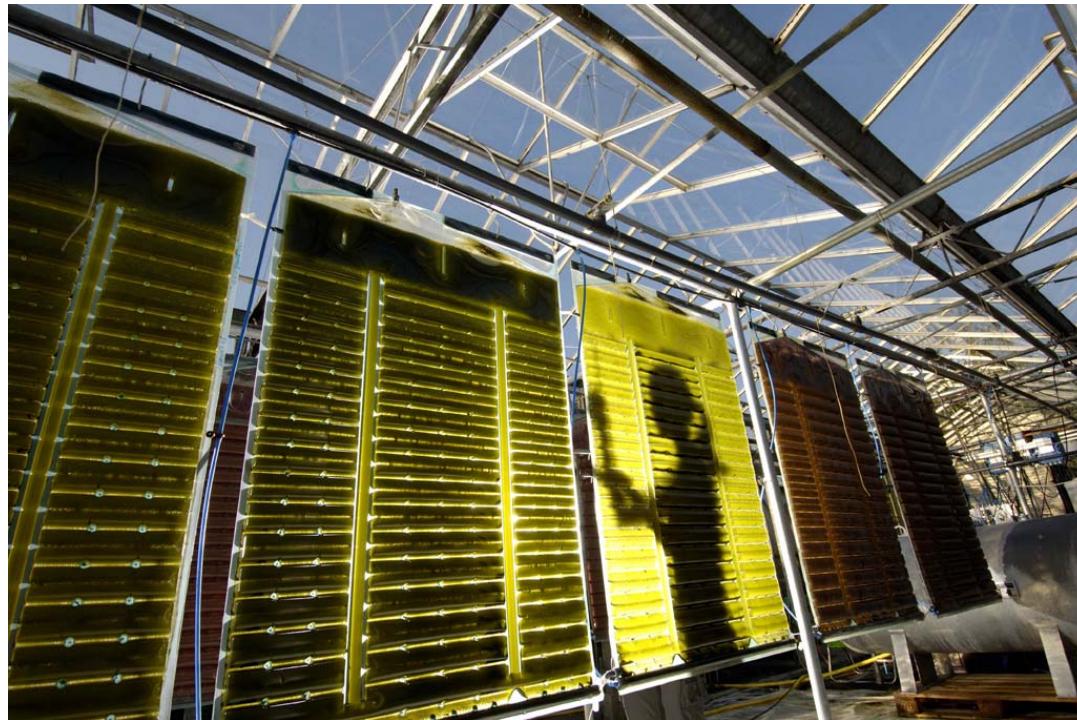
# **Energy efficiency and economics of the production of microalgae biomass with a flat panel-airlift photobioreactor**

**Dr. Peter Ripplinger  
Subitec GmbH**

# Content

- Subitec GmbH: the company
- Flat Panel Airlift (FPA) – Photobioreactor
- Pilot plants
- Integrated production process including Biorefinery
- Comparison of different production systems
- Economics of biomass production in industrial scale
- Summary

# Subitec GmbH: the company



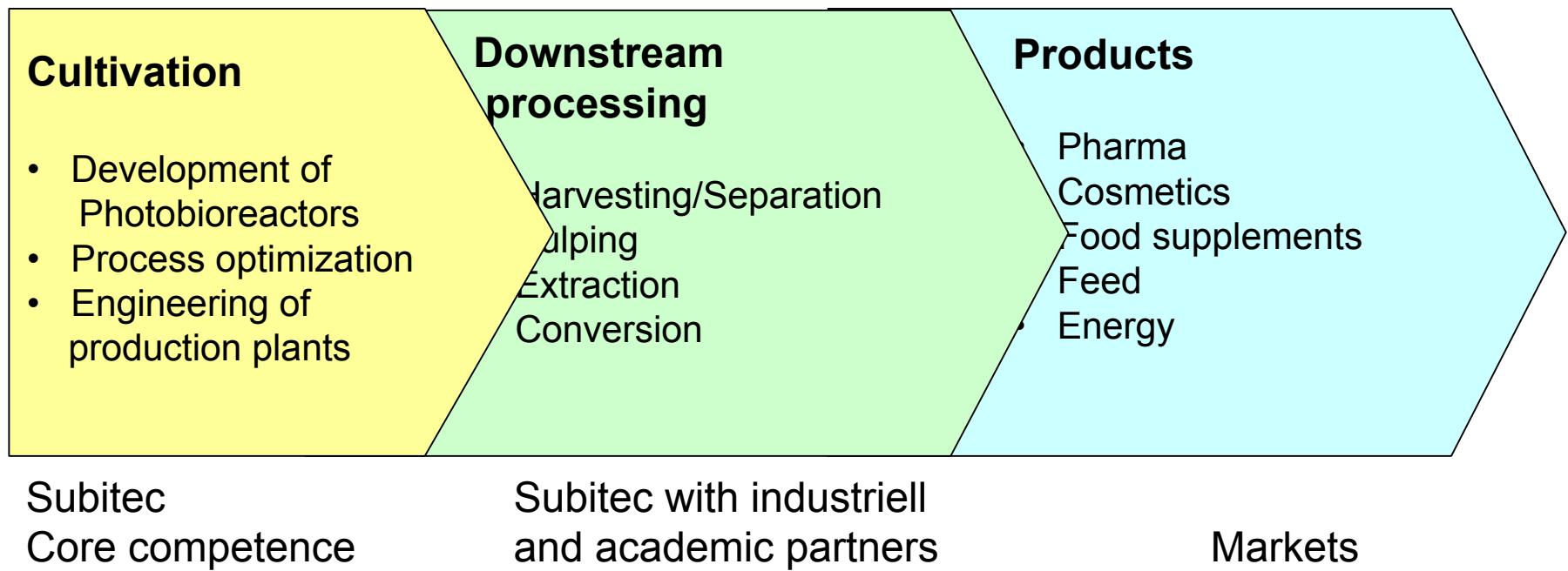
Pilot plant, Subitec GmbH, in Stuttgart-Vaihingen (2005)

# Subitec GmbH: the company

- Spin-off from the „Fraunhofer-Institut für Grenzflächen- und Bioverfahrenstechnik“ (IGB) in Stuttgart
- Two patent families regarding the Flat Panel Airlift- Photobioreactor granted worldwide
- Pilot plants with E.ON Hanse AG (in Hamburg) and EnBW AG (near Stuttgart)
- Projects funded by DBU (Deutsche Bundesstiftung Umwelt) the state Baden-Württemberg

# Position in the value chain

Product development with academic and industrial partners

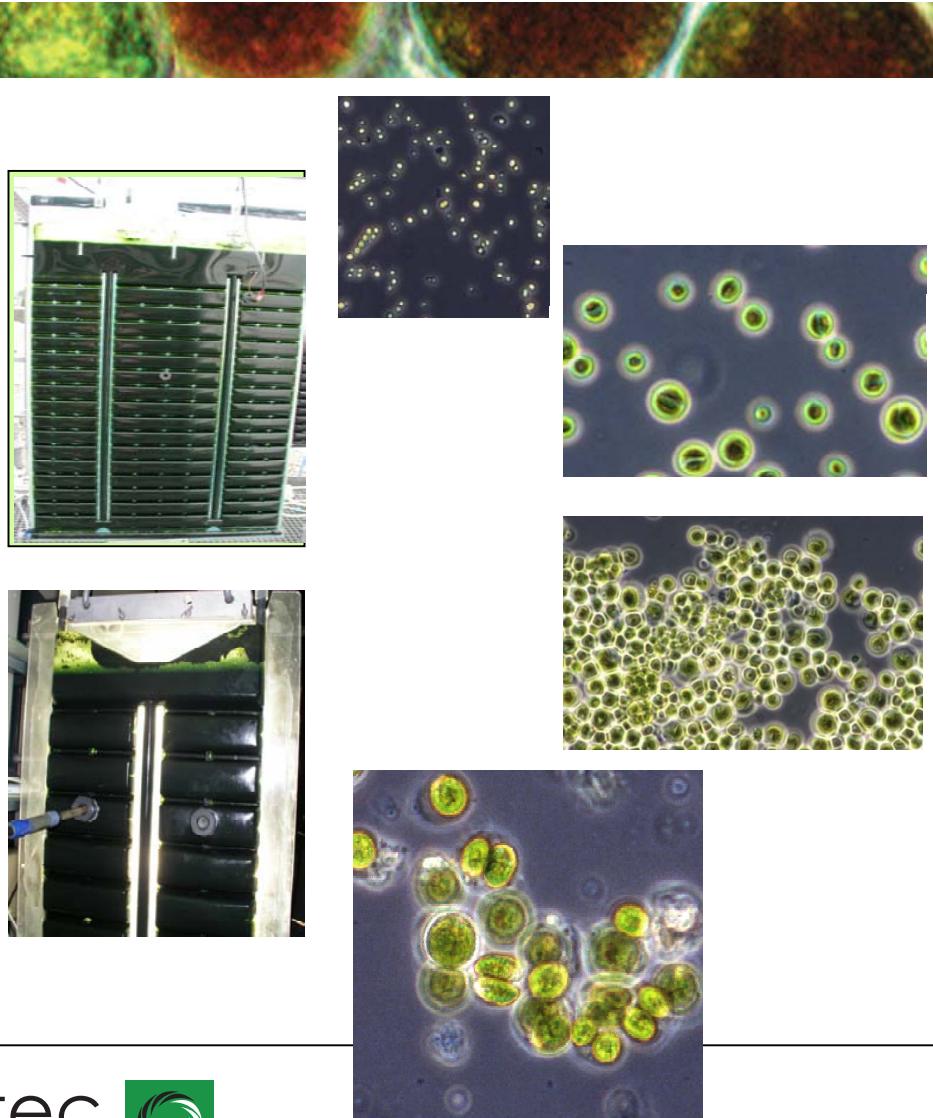


# Products and Services

- Systems for the cultivation of microalgae based on 5 L, 9 L, 33 L und 180 L-FPA-Reactors
- R&D partner for biorefinery concepts based on algae biomass
- Production of algae biomass for the cosmetic and pharma industry and for product development

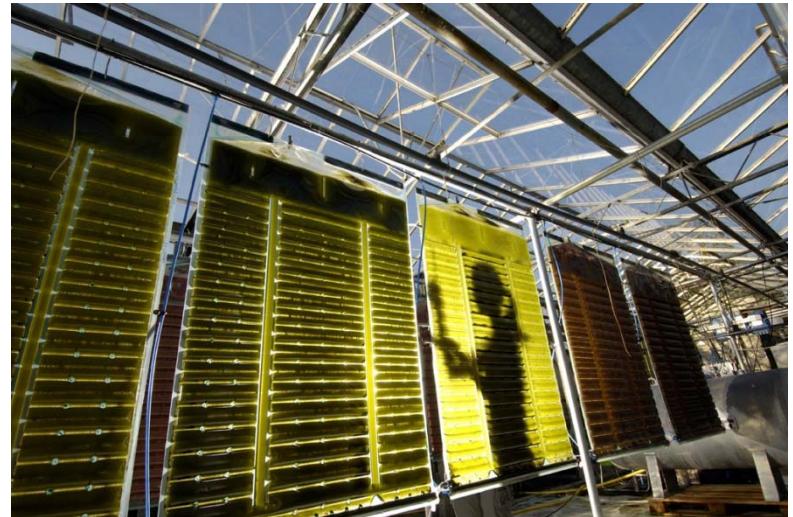
# Microalgae cultivated in the FPA-Reactor

Marine algae	Lab scale	
	max. DW (g/l)	Ø Prod. (g DW/l*d)
Isochrysis spec. (clone T.iso)	10	0,5
Nannochloropsis oculata	13	1
Tetraselmis suecica	16	0,6
Platymonas subcordiformis	12	0,5
Other algae (sweet water)		
Chlorella vulgaris	12	0,8
Chlorella sorokiniana	12	1,3
Eigenisolat DSN 5.1	16	0,7
Haematococcus pluvialis	2,5 <sup>a</sup>	0,5
	5 <sup>b</sup>	0,3
Phaeodactylum tricornutum	25 <sup>d</sup>	1,5
	12 <sup>e</sup>	0,9



# Flat Panel Airlift (FPA) – Photobioreactor

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Pilotanlage der Subitec GmbH in Stuttgart-Vaihingen (2005)

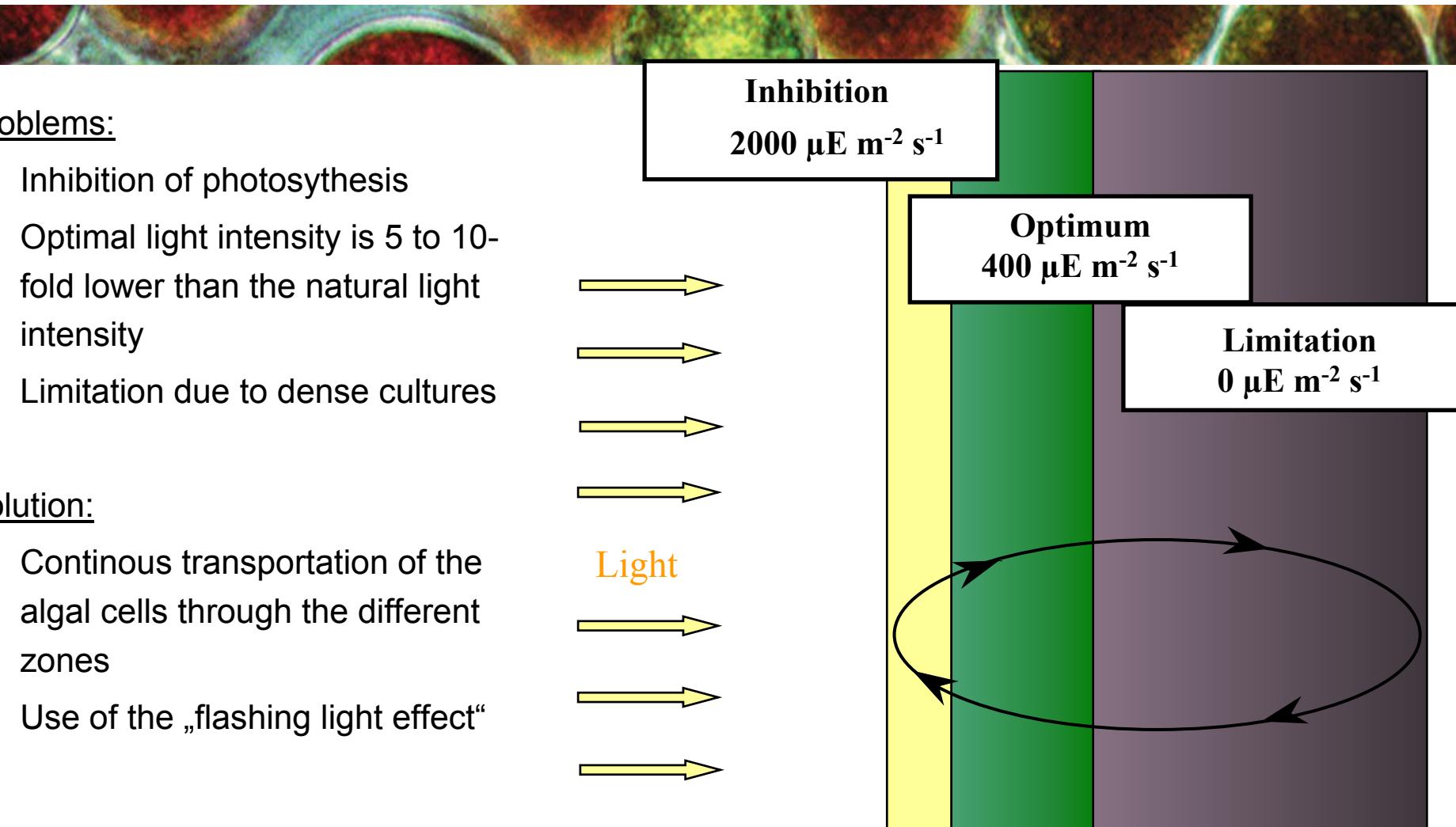
# Light supply in dense algae cultures

## Problems:

- Inhibition of photosynthesis
- Optimal light intensity is 5 to 10-fold lower than the natural light intensity
- Limitation due to dense cultures

## Solution:

- Continuous transportation of the algal cells through the different zones
- Use of the „flashing light effect“



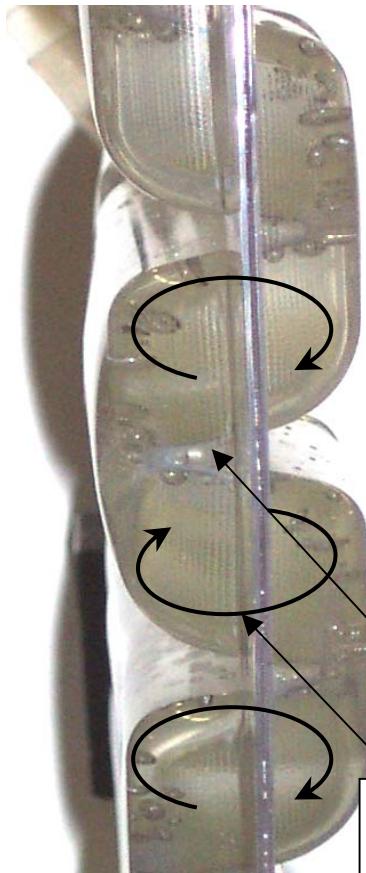
# FPA technology

## Process engineering

- efficient light supply to all cells
- complete homogenous intermixing
- low mechanical stress to the cells
- simple temperature and pH control
- efficient gas exchange

## Cost-effectiveness

- high volumetric productivity
- high cell densities
- high reactor volumes
- low capital and operating costs
- high reliability

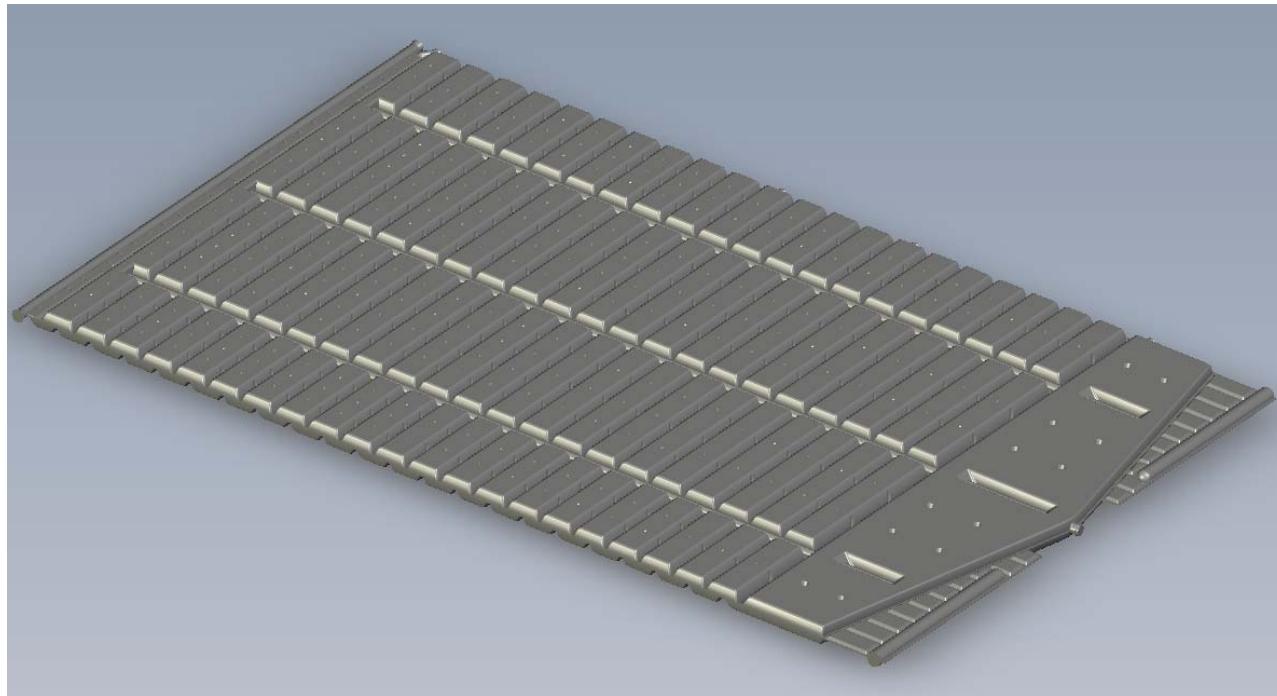


Halfshells of the FPA made from deep-drawn plastic sheets



static mixers  
flow

# FPA-Reactor, 3. Generation (2008)



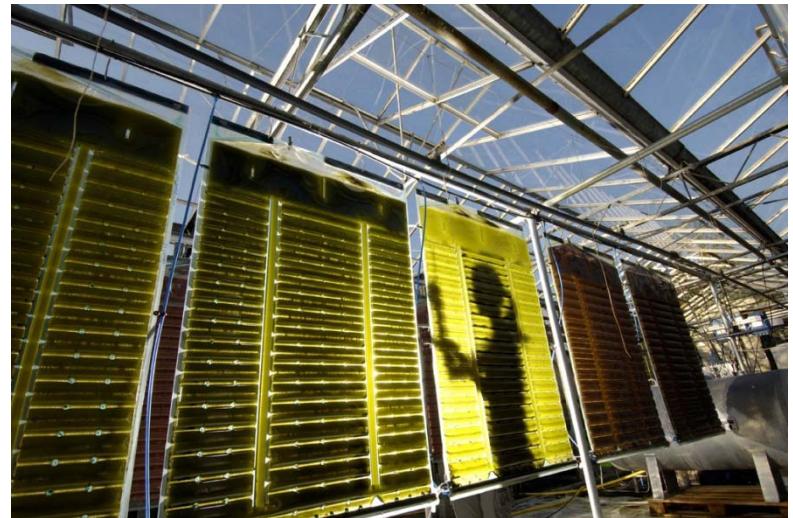
<u>Technical data:</u>	Hights	270 cm	Volume	180 l
	Lengths	175 cm	Material	PVC or
	Thickness	5 cm		PETg

# Advantages of the new FPA - Reactor

- 
- Reduction of production costs of the bioreactor  
(ca. 1.000 €/m<sup>3</sup>)
  - Could be used over a 5 year period (new materials)
  - No problems with leakages (Twin-Sheet technology)
  - Reduction of the energy consumption  
(from 477 W/m<sup>3</sup> to 100 - 200 W/m<sup>3</sup>)

# Pilot plants

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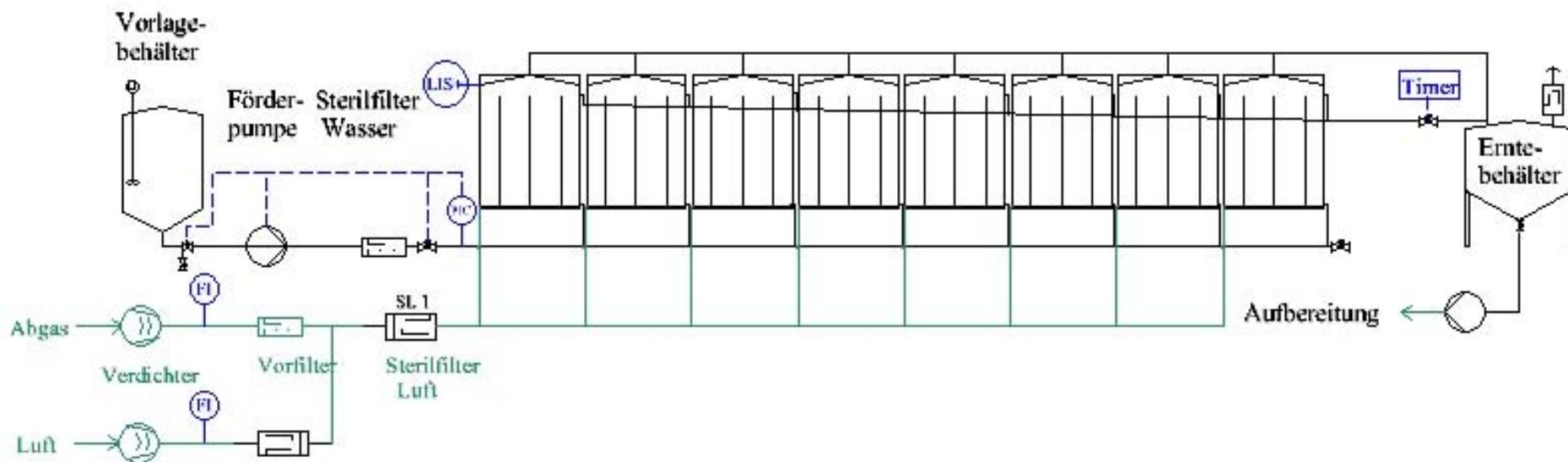


Pilotanlage der Subitec GmbH in Stuttgart-Vaihingen (2005)

# Pilot plants

- 
- since 2005: Pilot plant in Stuttgart-Vaihingen, based on 33 L-Reactors for the cultivation of Haematococcus and Phaeodactylum
- May 2008: Start of the pilot plant in Eutingen-Weitingen  
Multipurpose plant, based on 180 L-Reactor,  
Total volume: ca. 4 cbm
- June 2008: Start of the pilot plant in Hamburg-Reitbrook,  
two modules with 4 x 180 L-Reactors
- 2009: Pilot plant in a greenhouse (4 modules of 6 x 180 L-Reactors ),  
Production plant with 180 cbm total volume,  
ca. 0,5 – 0,7 ha, in Spain

# Flow chart – production modul



# Subitec GmbH



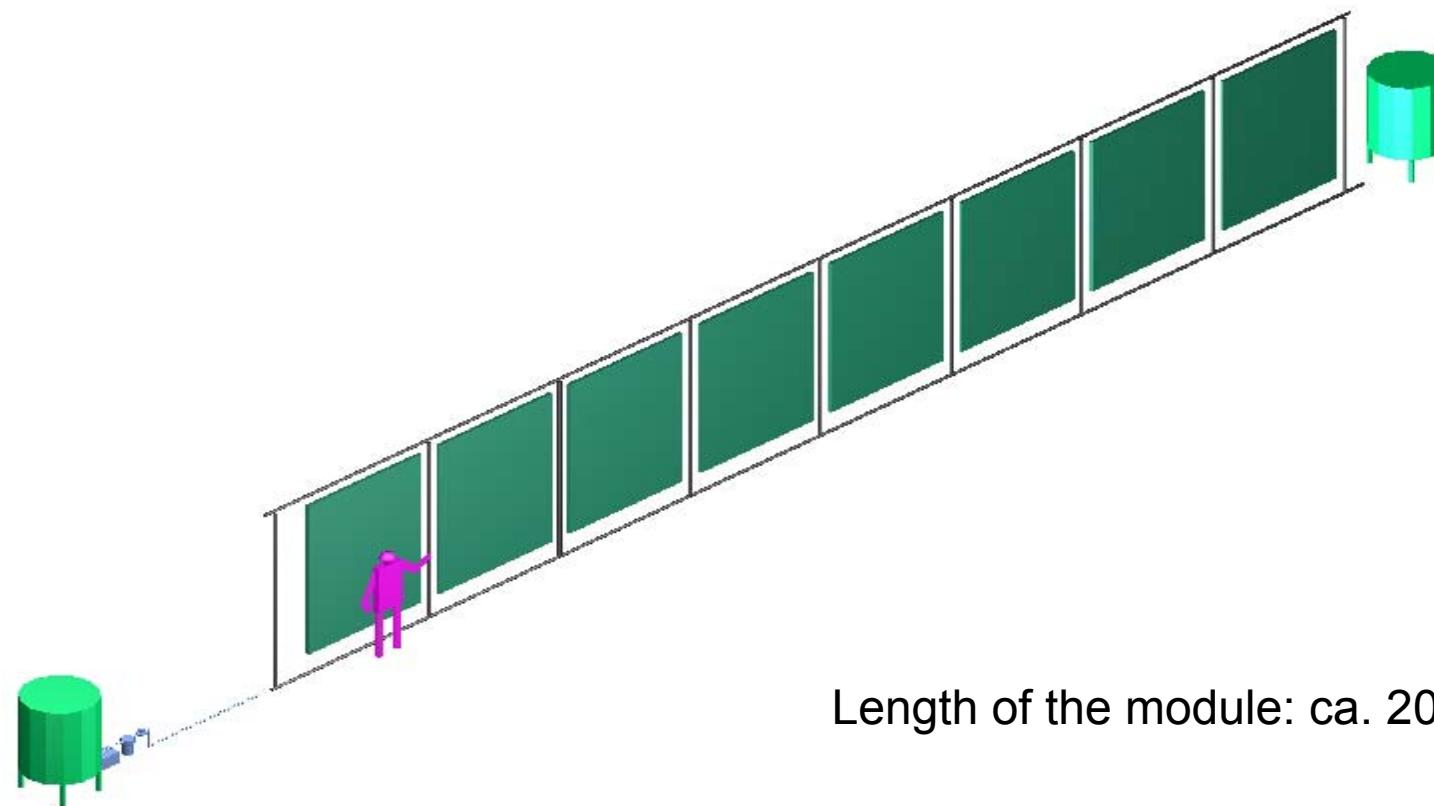
Pilot plant in Eutingen-Weitingen (2008)

# Subitec GmbH



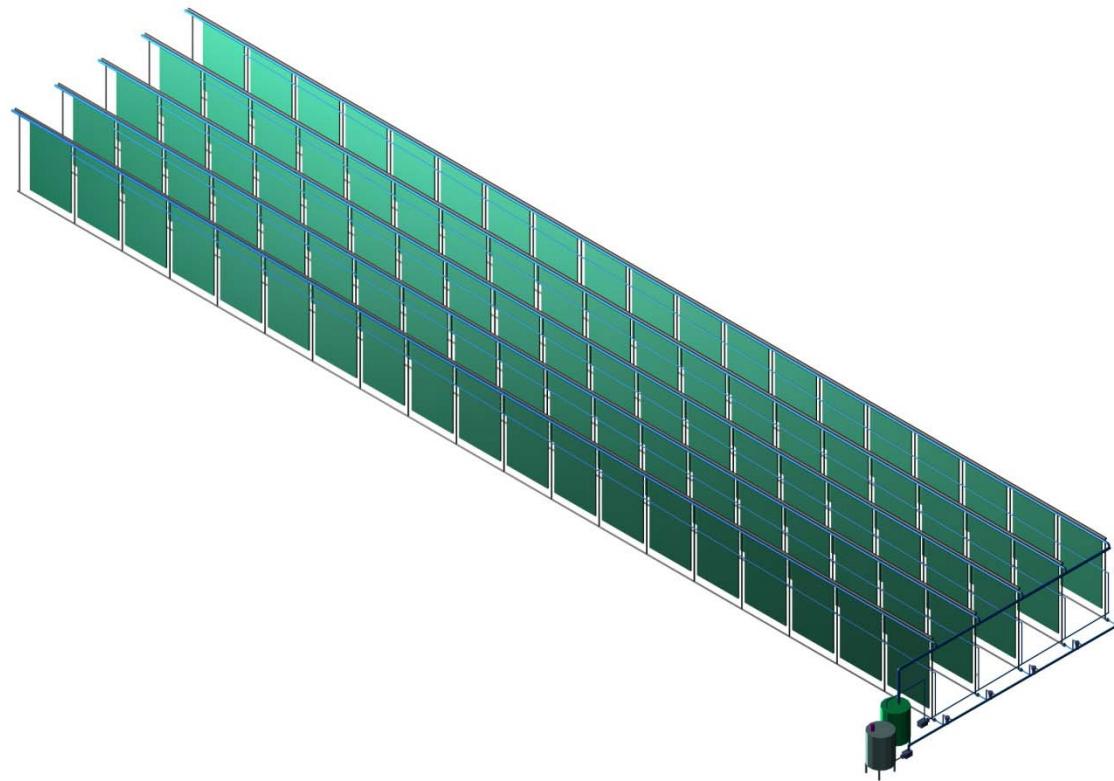
Pilot plant in Hamburg-Reitbrook in cooperation with E.ON Hanse (2008)

# Modul with 8 x 180 L FPA reactors

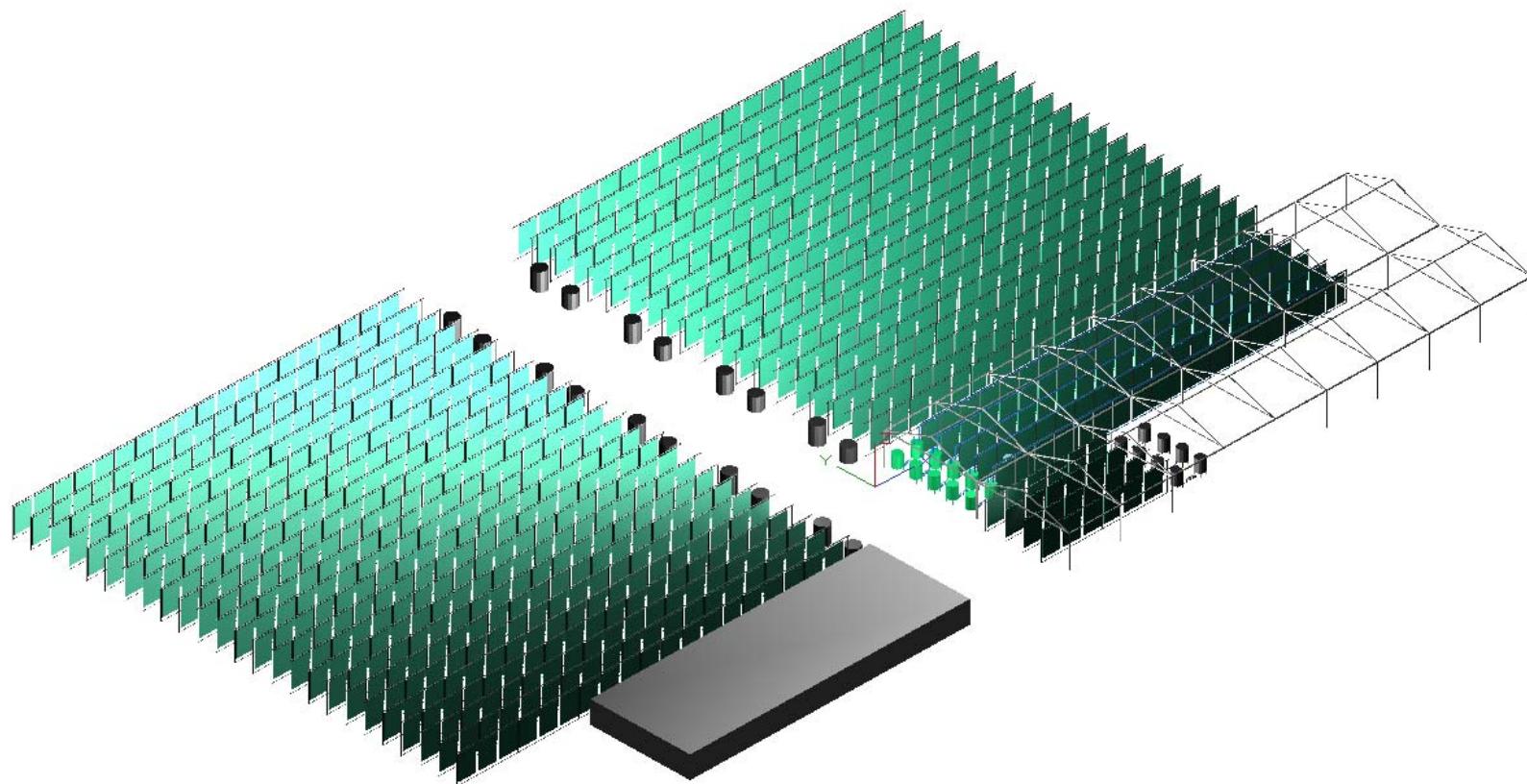


Length of the module: ca. 20 m

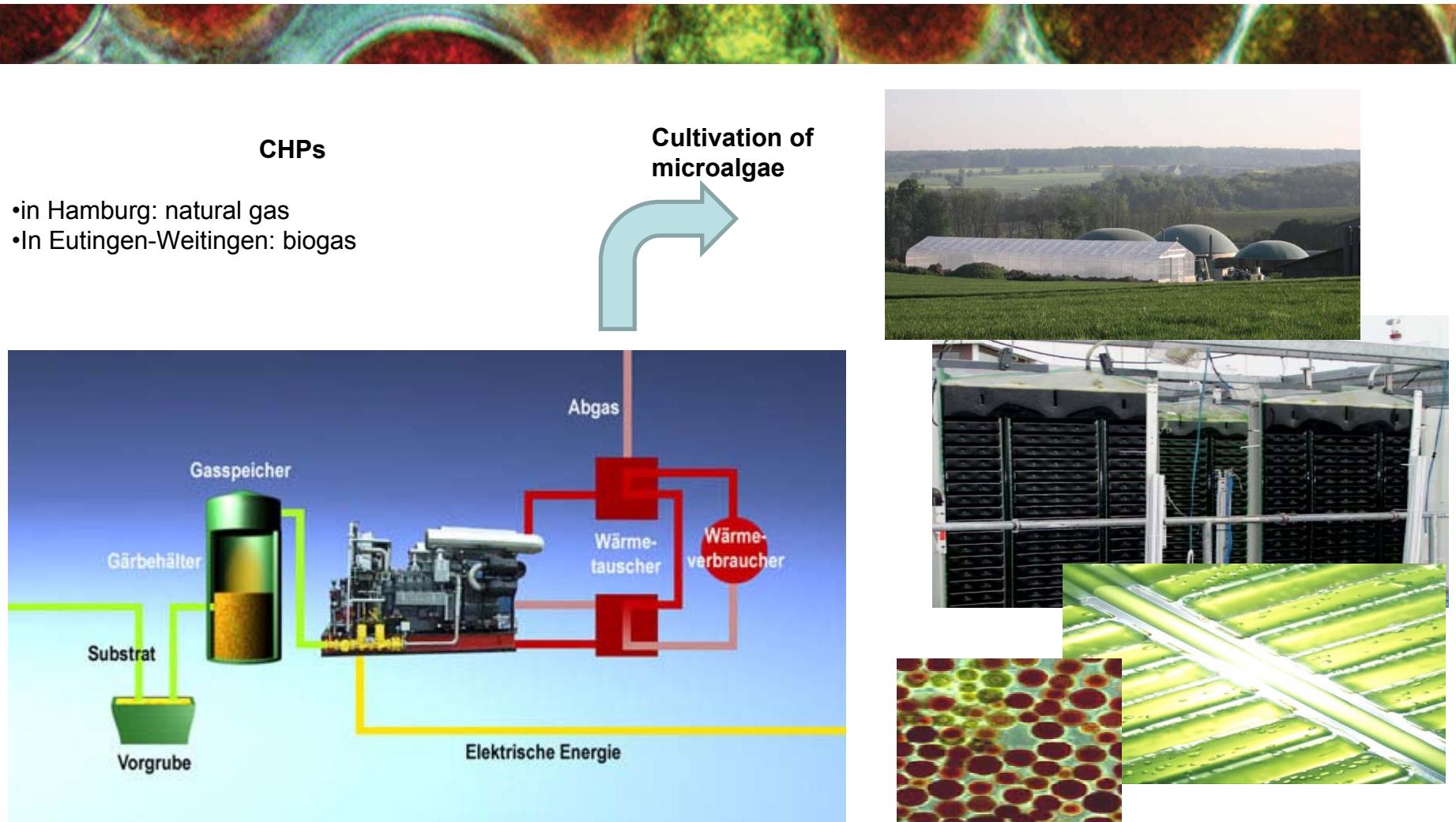
# Sceme of a 5 x 20 module



# Pilot plant in Spain (180 m<sup>3</sup>)

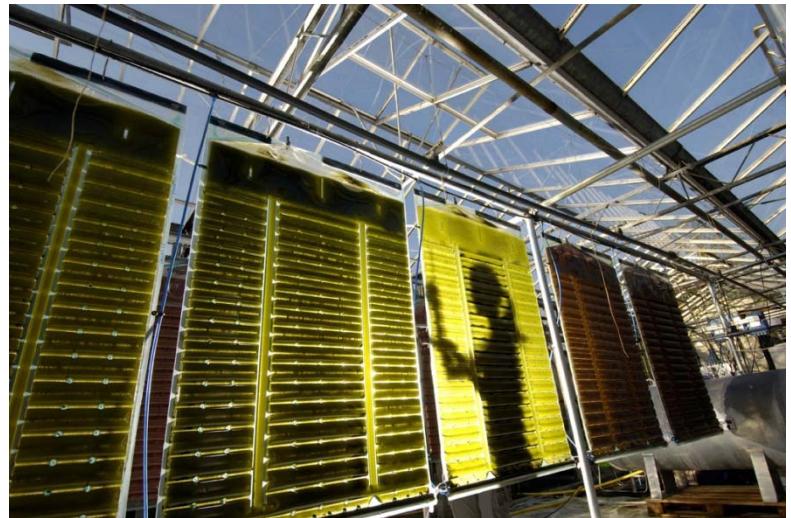


# Basic process of the pilot plants



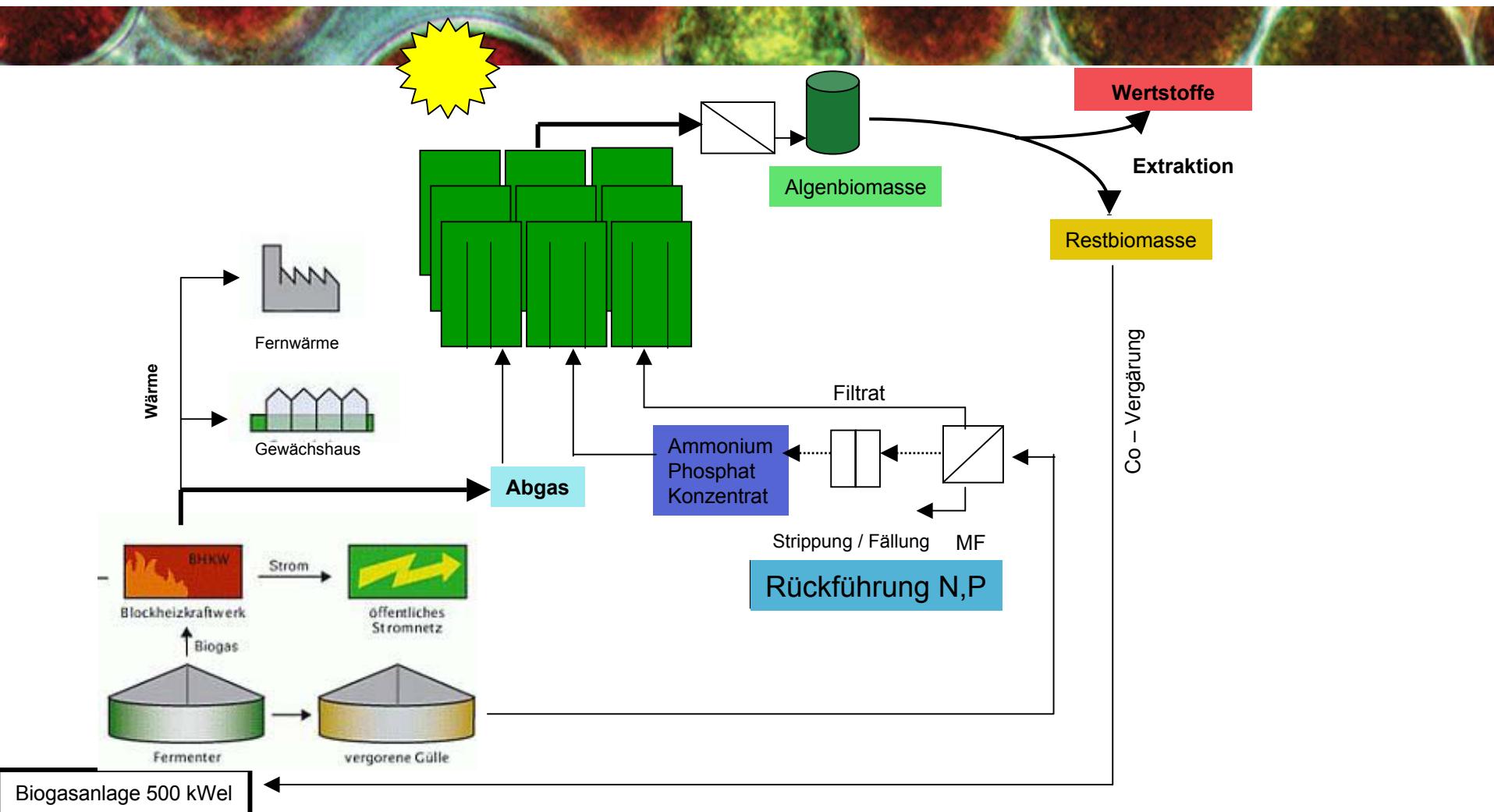
# Integrated production process including biorefinery

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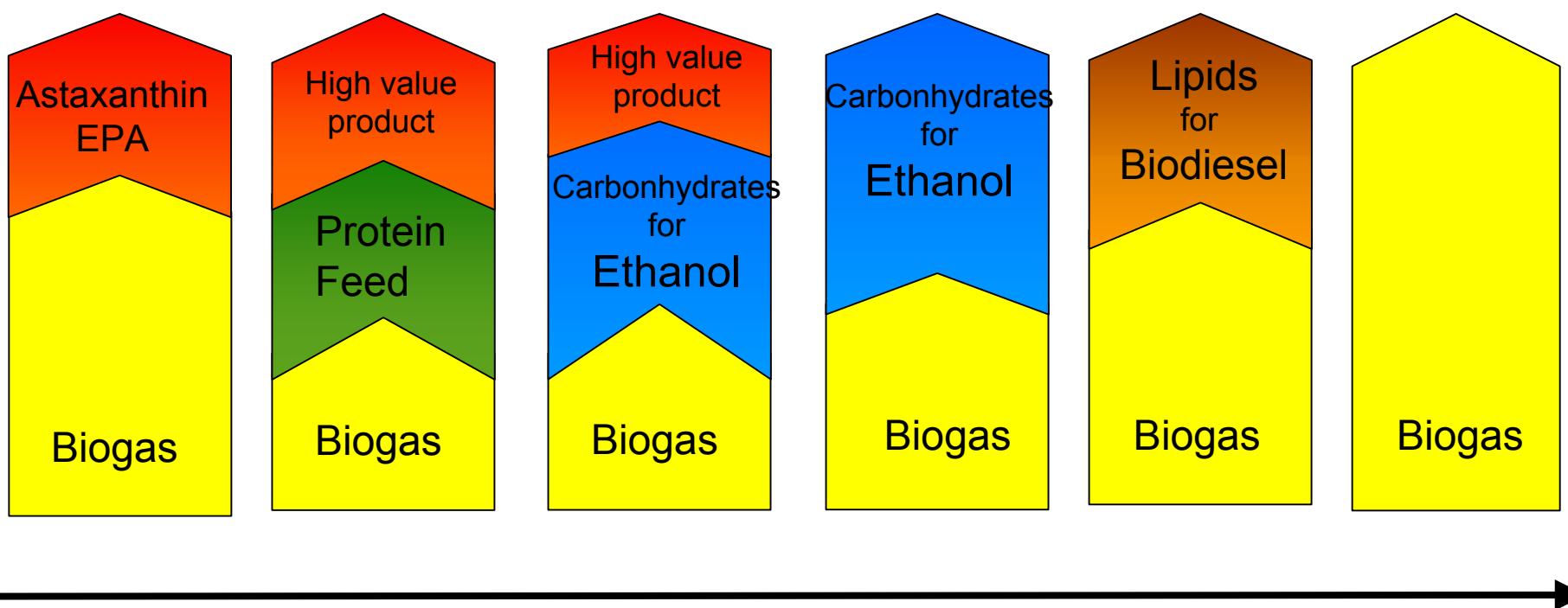


Pilotanlage der Subitec GmbH in Stuttgart-Vaihingen (2005)

# Integrated production process for microalgae biomass

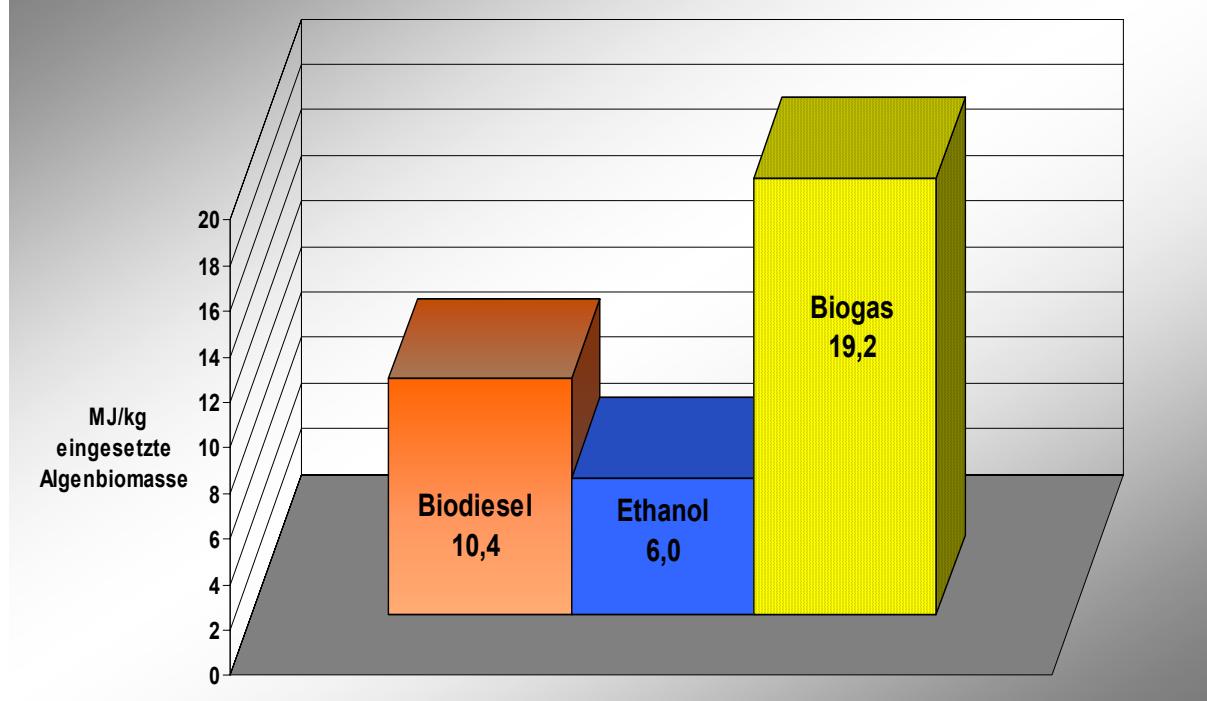


# Biorefinery concepts for algae biomass



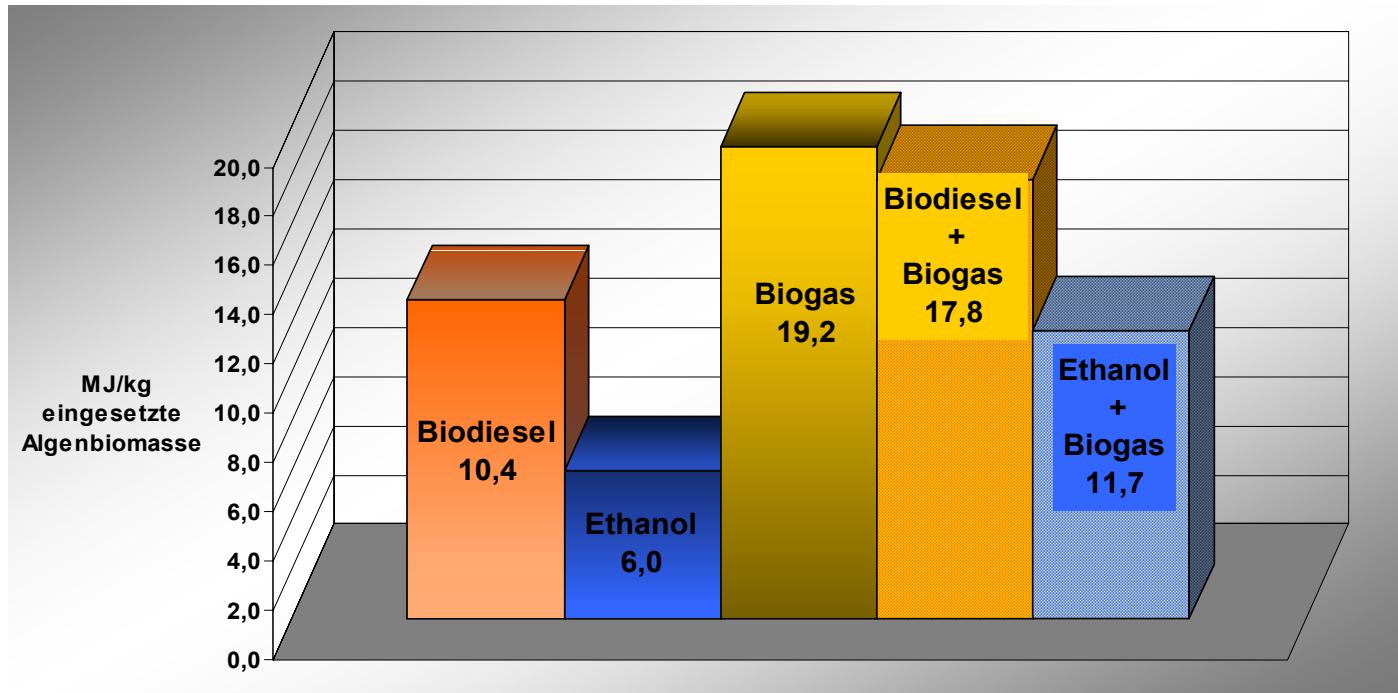
increasing energetical usage

# Total energy content of products derived from 1 kg algae biomass



- 35 % of lipids to produce 0,35 kg FME
- 50 % of carbohydrates to produce 0,225 kg of ethanol
- 0,8 m<sup>3</sup> of biogas derived from 1 kg dry algae biomass

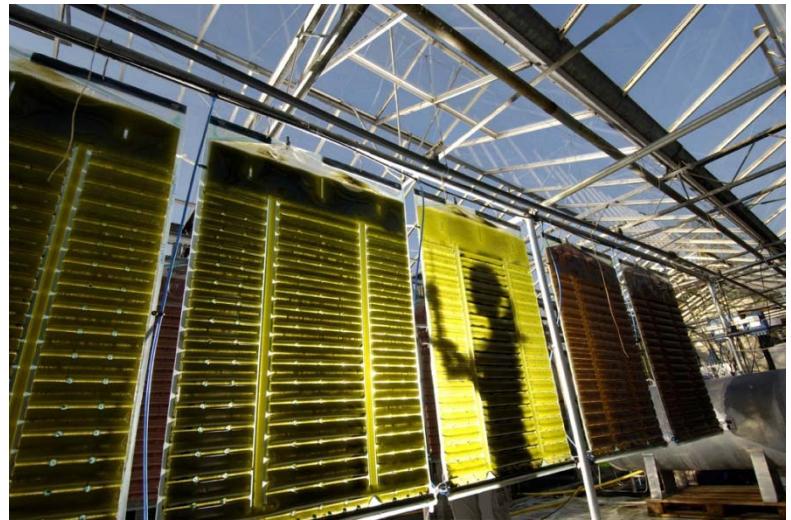
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# Comparison of different production systems

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# Is net energy production achievable?

A microscopic image showing several green, circular algae cells with distinct internal structures and some red/orange pigmentation.

Energy content of algae biomass

- energy input for cultivation
- 

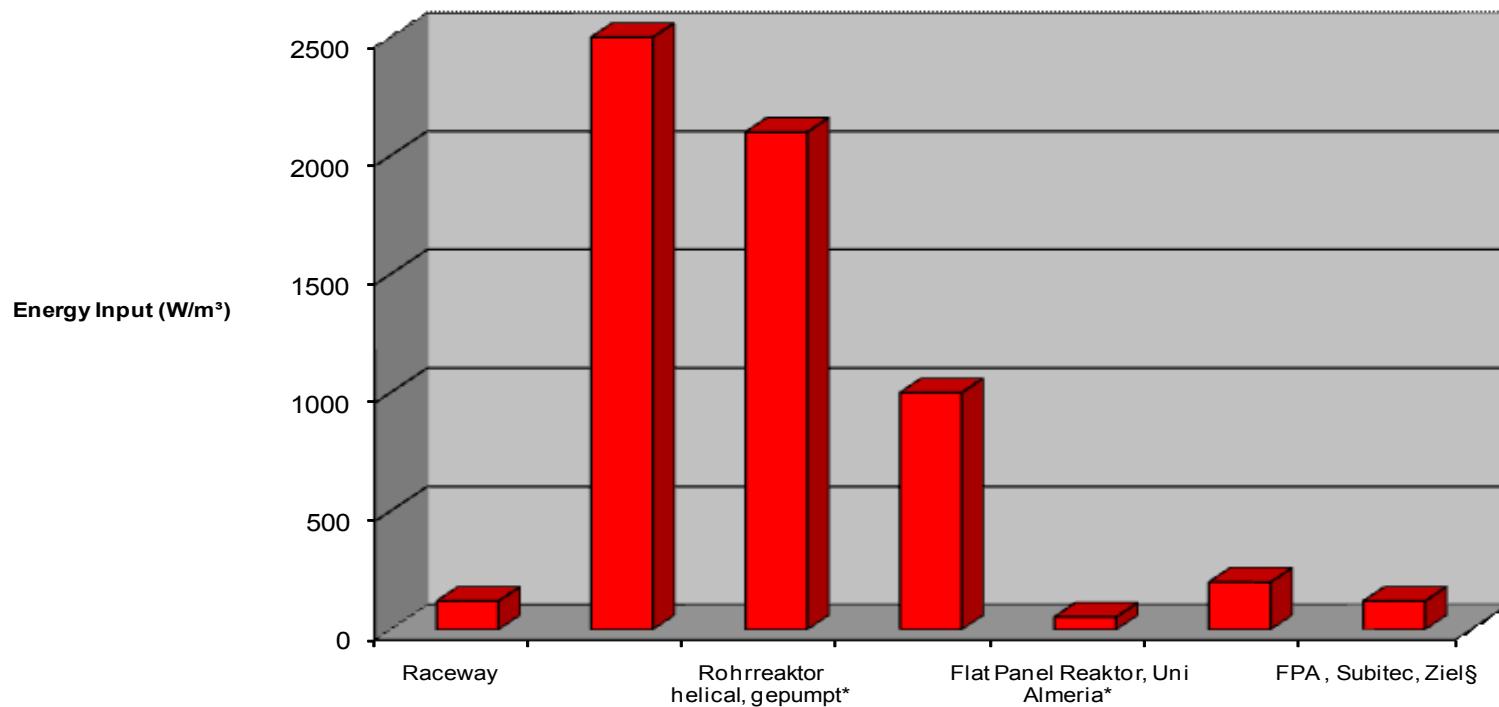
Net energy production ???

# Comparison of different culture systems



	Open ponds	Tubular	Flat-Panel-Airlift-Reaktor (FPA)
<b>Risk of contamination</b>	high	low	low
<b>Volumetric productivity</b>	low	medium/high	high
<b>Cell density</b>	very low	medium/high	high
<b>Energy input</b>	low	high	low
<b>Capital costs</b>	low	high	medium

# Comparison of the energy input of different production systems

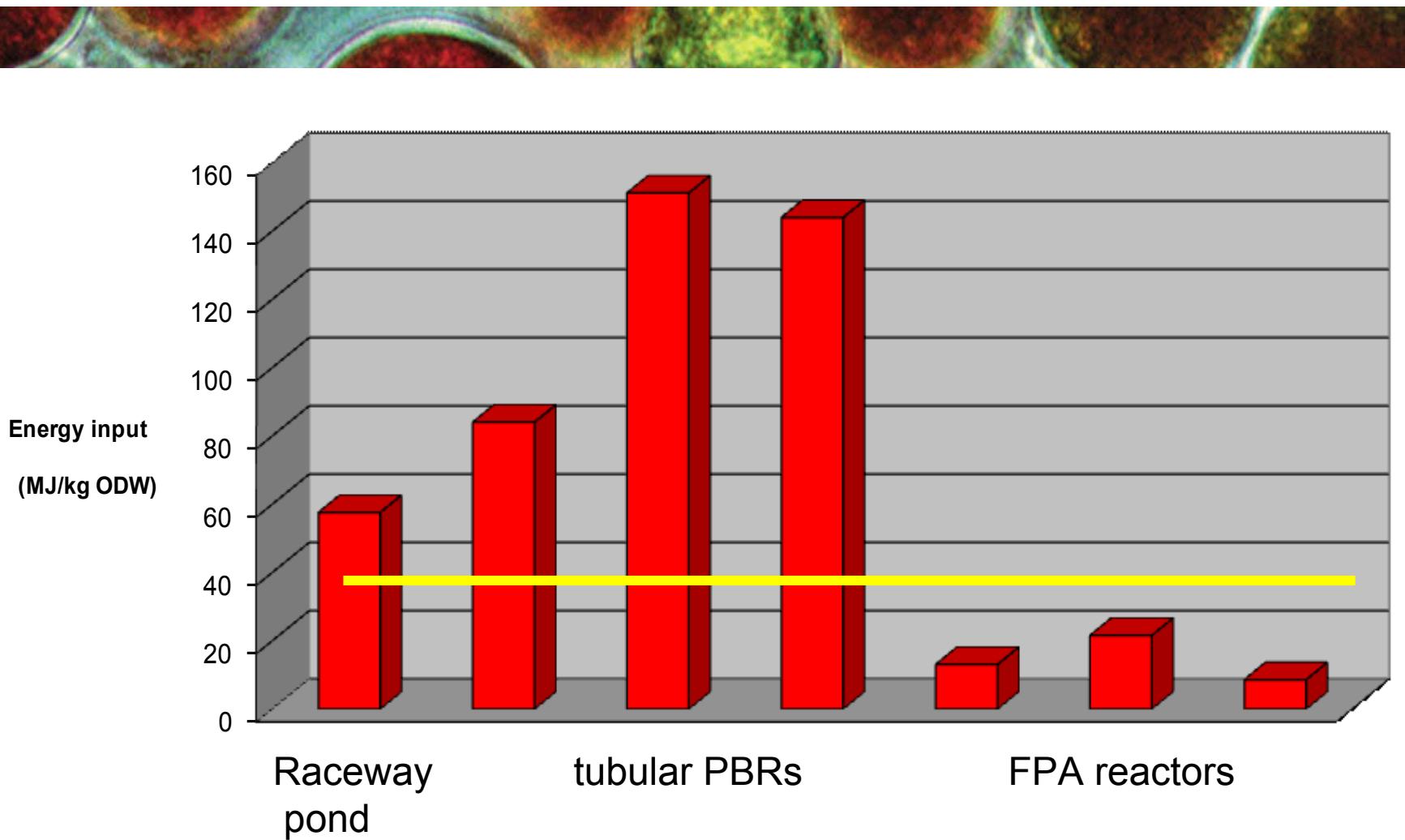


\* Daten aus Sierra et al. 2007

\*\* abgeschätzt nach Angaben Pumpenleistung, IGV

§ Angaben für 165 L-FPA

# Comparison of the energy input per kg DW of different production systems



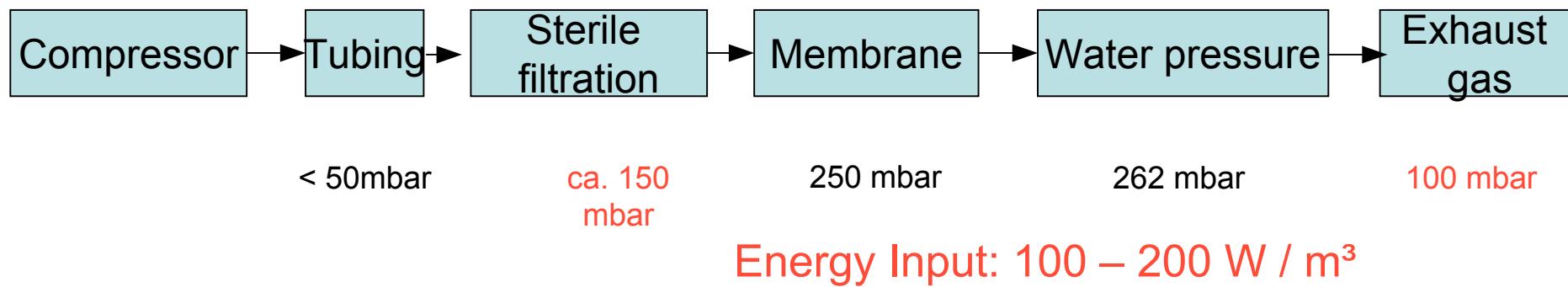
# Net energy production is achievable!

It can be proven  
that a net energy production is only achievable with  
a Flat Panel Airlift-Bioreactor system.



# Pressure losses for the FPA-System

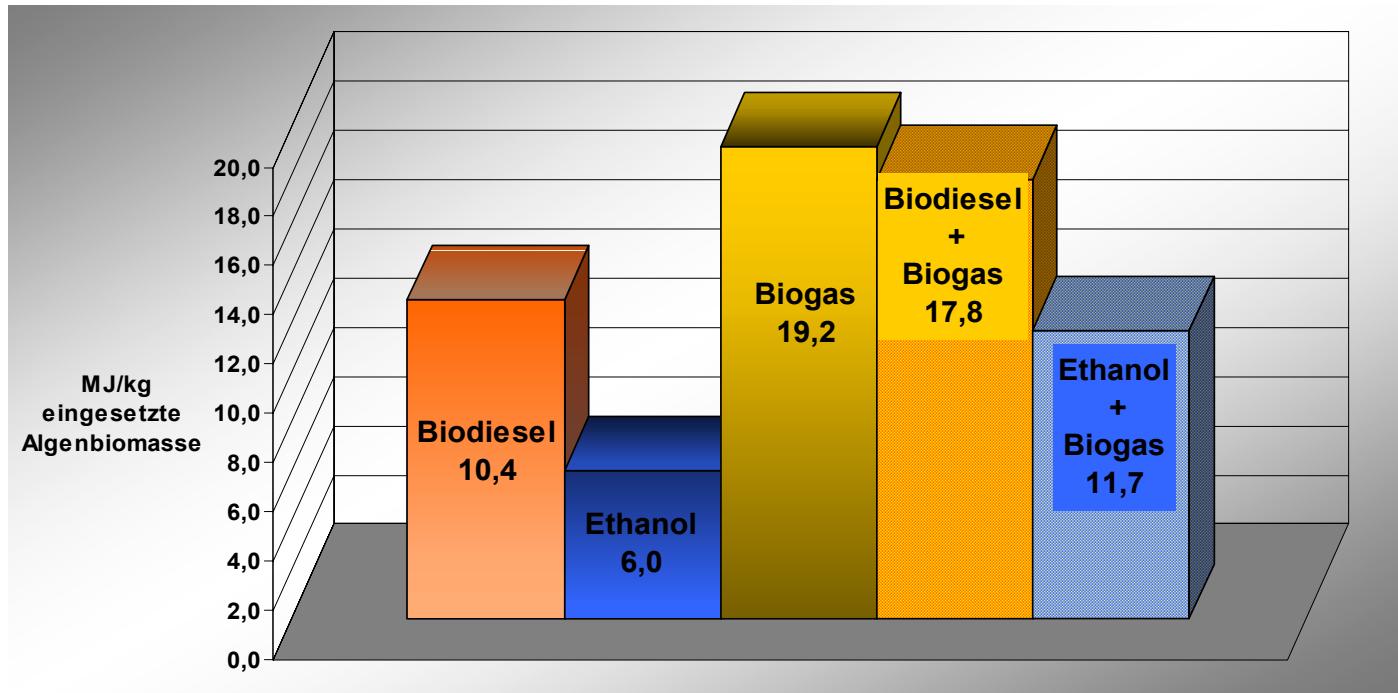
Total working pressure = Sum of partial pressure losses



Possible optimisations:

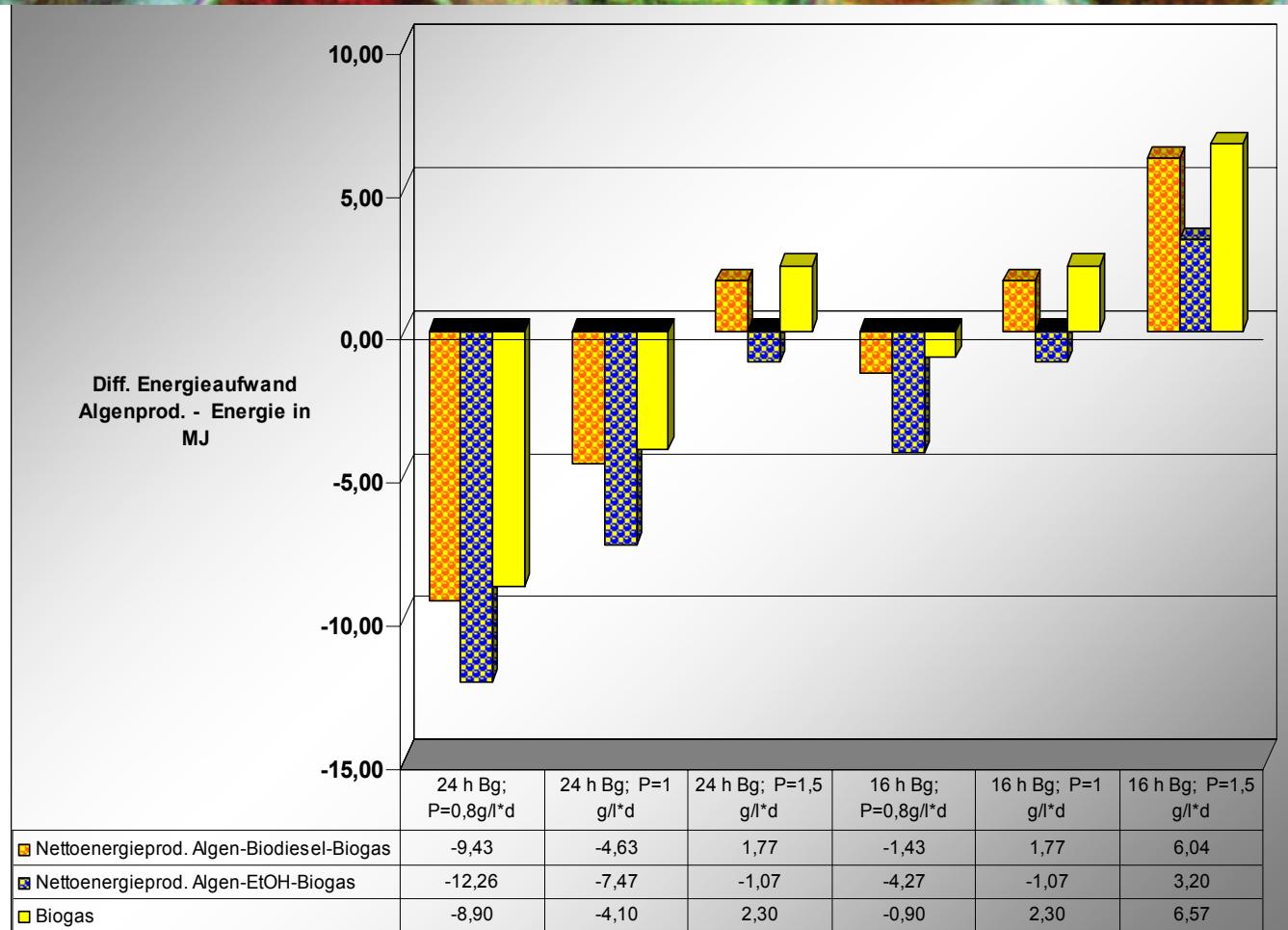
1. Membrane
2. robust algae cultures / mixed cultures
3. Use of industrial processes, which deliver CO<sub>2</sub> under pressure
4. Airflow adapted to light intensity/actual productivity

# Total energy content of product derived from 1 kg algae biomass

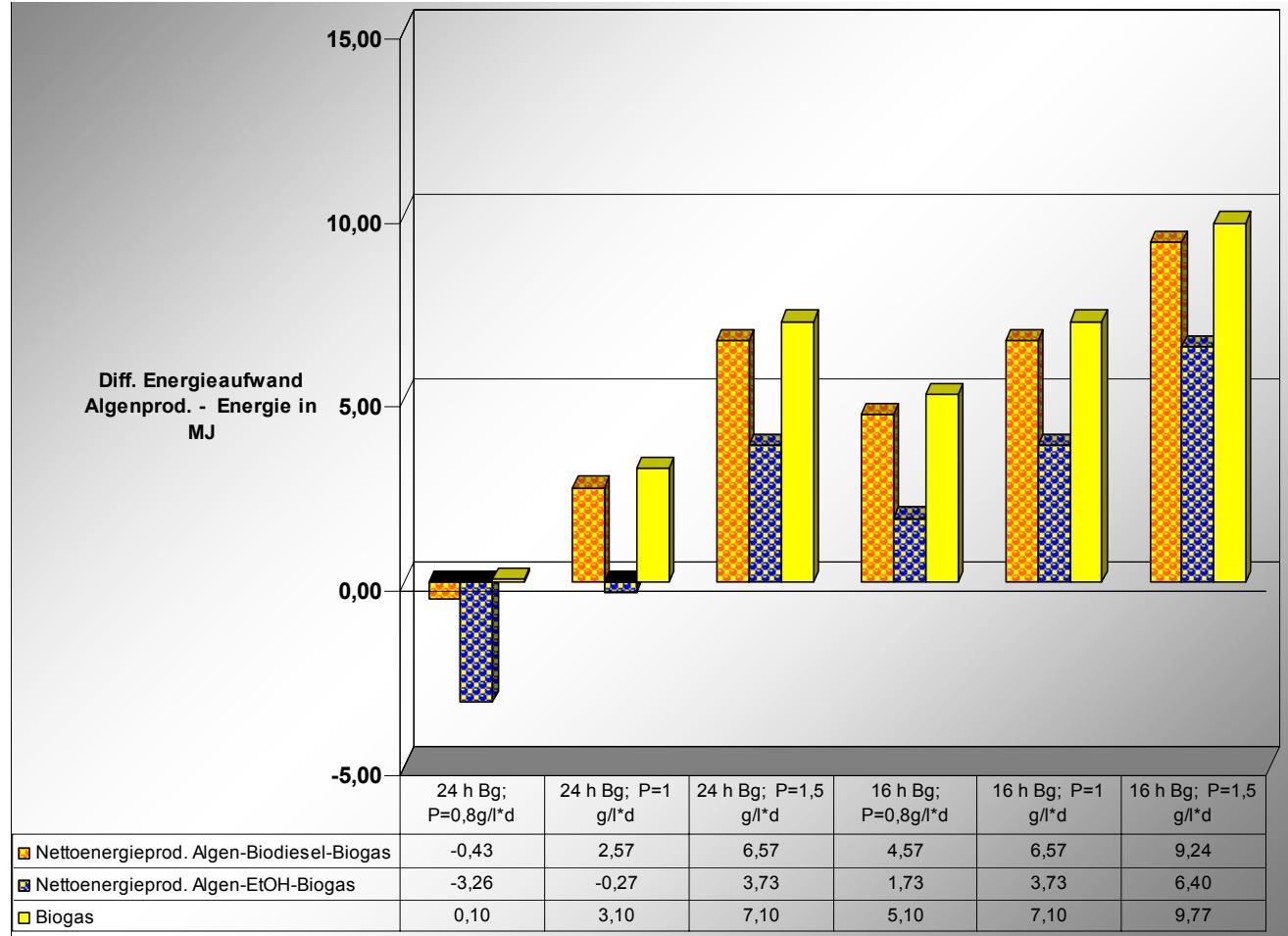


- 35 % of lipids to produce 0,35 kg FME
- 50 % of carbonhydrates to produce 0,225 kg of ethanol
- 0,8 m<sup>3</sup> of biogas derived from 1 kg dry algae biomass

# Net energy gain with FPA at 0,8 bar working pressure

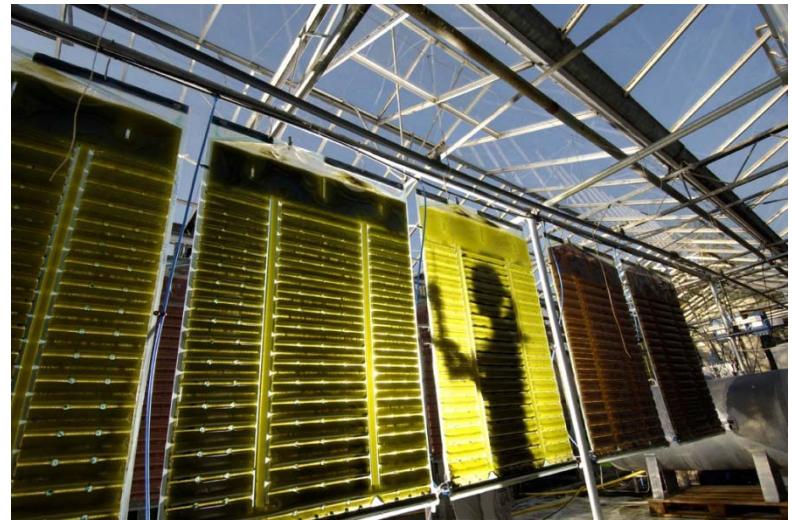


# Net energy gain with FPA at 0,5 bar working pressure



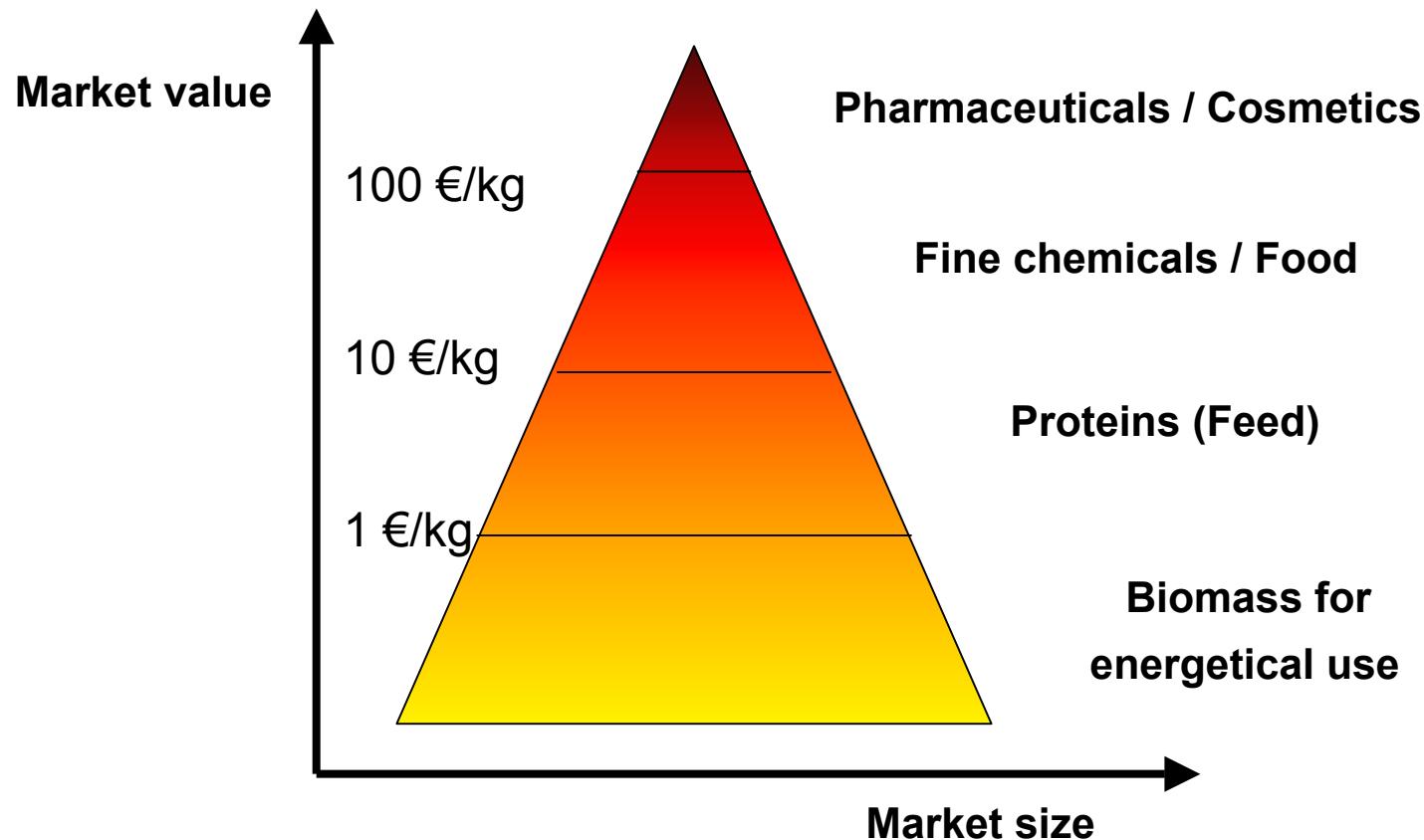
# Economics of biomass production in industrial scale

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Pilotanlage der Subitec GmbH in Stuttgart-Vaihingen (2005)

# Value and market size for algae biomass in different market segments



# Annual productivity in different climates

climatic zone	productive days per year	Productivity per ha and year (t DW / ha*a)	
		with ø 1g DW/l*d	with ø 0,8 g DW/l*d
tropical	365	137	110
Mediteranee	300	113	90
central europe	240	90	72
Stuttgart	200	75	60

Calculated for the 180 L-FPA and 2,50 m distance between the modules

productivity > 100 t TS / ha \* year

# Production and capital costs

**For a 1 ha plant:**

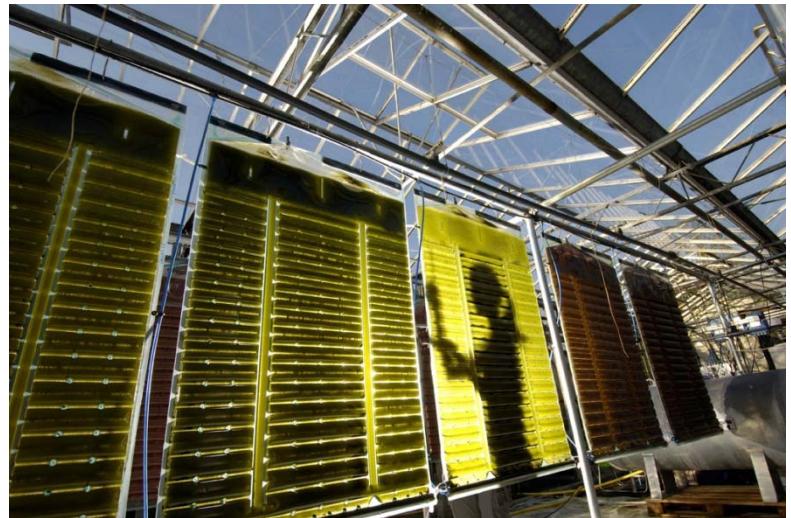
- capital costs 1'500'000 € (25% for FPA-photobioreactors)
- productivity 120 t / year
- production costs:

Depreciation	2.000	€ / t ODW
Electricity	200	€ / t ODW
Nutrients	1.500	€ / t ODW
Personnel costs	500	€ / t ODW
Total (incl. dep.)	4200	€ / t ODW

**For a 100 ha plant: ????**

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# Summary

- Third generation FPA-Reactors is available since 2008
- 2 pilot plants started operation in 2008
- At least 4 pilot plants are planned for 2009
- Capital costs and running costs for production plants could be diminished radically
- Net energy gain is possible
- Production of fine chemicals in large scale is possible today
- Production of algae biomass for feed, lipid production and for energetical use is achievable in 3 – 5 years



Thanks for your kind attention!

